





# Exhaust gas aftertreatment modelling: a focus on the NH<sub>3</sub>-SCR of NO<sub>x</sub> from Diesel vehicles

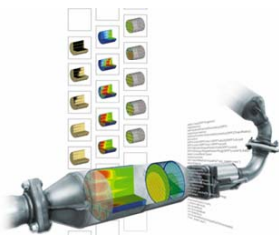

**Massimo Colombo**  
ESR at LAT/AUTH, Nov. 2010 - June 2011

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## Personal Background

- **Project:** EC Marie Curie FP7 ITN **VECOM** (Oct 2008 - Sept. 2012)
- **Massimo Colombo (ESR, from Italy)** <http://www.vecom.org>
  - Born on September, 24<sup>th</sup> 1984
  - M.Sc. in Chemical Engineering at Politecnico di Milano, December 2008;
  - Internship at DAIMLER A.G., Oct. 2007/March 2008 (6 months);
  - Ph.D. Student at Dipartimento di Energia - Politecnico di Milano, Jan.2009/Dec.2011;
  - ESR for EC Marie Curie FP7 ITN “VECOM” at Laboratory of Applied Thermodynamics, Aristotle University of Thessaloniki, Greece (Nov. 2010-May 2011)
  - 11 communications to international conferences
  - 4 journal papers
- **Research Topics:**
  - Mechanism, kinetics and modeling of Ammonia Selective Catalytic Reduction (SCR) of NO<sub>x</sub> from diesel exhausts
  - Diesel exhausts aftertreatment modeling

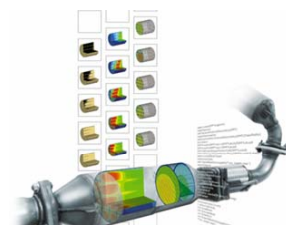
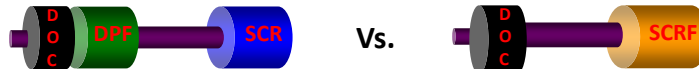
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## Research activity at LAT

**METHODS:** Simulation studies by means of an exhausts systems simulation platform, axisuite®, developed at LAT/AUTH over the last 15 years and further developed and supported by Exothermia SA

**TOPICS:**

- ✓ **Simulation study of Selective Catalytic Reduction on Filters (SCRf) systems**
  - To ZEV symposium (June 9-10, 2011, Turin, Italy):  
Oral Presentation + SAE Technical Paper (2011-37-0031)
- ✓ **Simulation of Ammonia Slip Catalysts (ASC)**
  - 2011 CLEERS workshop (April 19-21, 2011, Detroit – MI, U.S.A.)  
Oral Presentation + future publication in peer-reviewed journal
- ✓ **Modeling of ammonia adsorption over zeolite based catalysts**
  - MODEGAT II (September 19-20<sup>th</sup>, 2011)  
Poster presentation + eventual publication in peer-reviewed journal

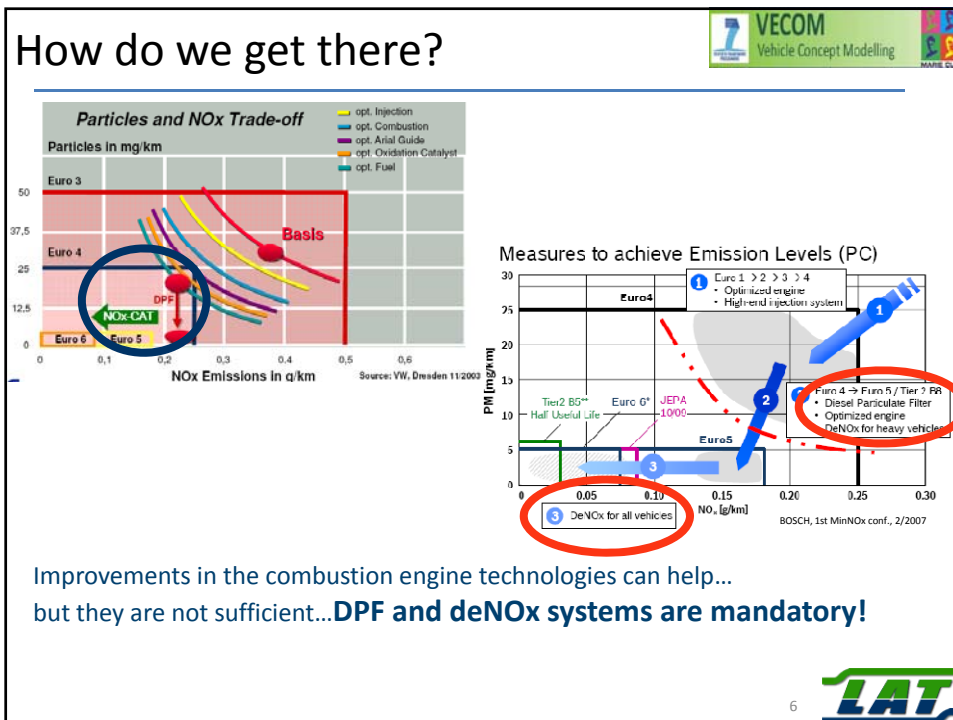
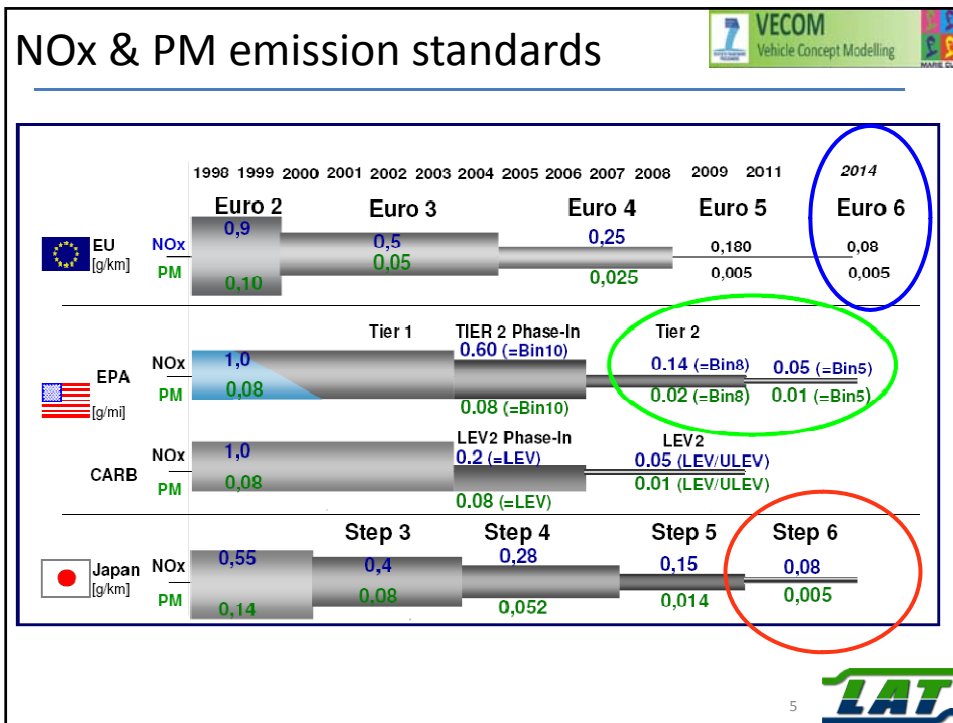



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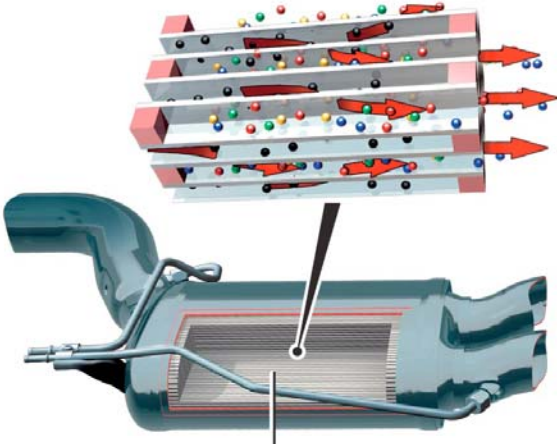
## Outline

- **Background**
  - NOx & PM emission regulations for Diesel vehicles
  - NH<sub>3</sub>-SCR & DPF technologies
- **Methods**
  - Simulation tools: axisuite®
- **Simulation results**
  - Selective Catalytic Reduction on Filters (SCRf) systems
  - Dual-Layer Ammonia Slip Catalysts (ASC)

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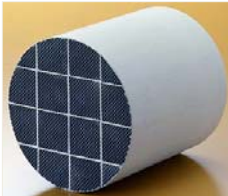

## DPF systems





- Plugs at channel outlets
- Wall porosity

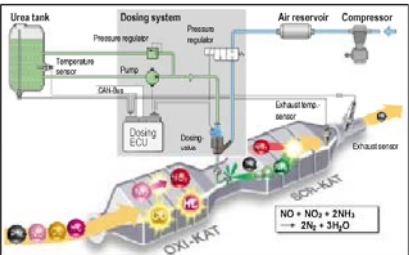
Cyclic operation: filtration & regeneration

<http://www.ngk.co.jp>, <http://www.theautochannel.com>

## NH<sub>3</sub>-SCR systems






$4\text{NH}_3 + 4\text{NO} + \text{O}_2 \rightarrow 4\text{N}_2 + 6\text{H}_2\text{O}$	<b>Standard SCR</b>
$2\text{NH}_3 + \text{NO} + \text{NO}_2 \rightarrow 2\text{N}_2 + 3\text{H}_2\text{O}$	<b>Fast SCR</b>
$4\text{NH}_3 + 3\text{NO}_2 \rightarrow 3.5\text{N}_2 + 6\text{H}_2\text{O}$	<b>NO<sub>2</sub>-SCR</b>

- On-board NH<sub>3</sub> source → aqueous solution of urea
- DOC upstream of the SCR converter (NO→NO<sub>2</sub>)

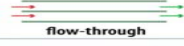


### Open issues

- 1) Enhanced Low-T activity of the SCR reactions → NEW CATALYSTS
- 2) Reaction pathways, catalytic mechanism, kinetics, role of NO<sub>2</sub>
- 3) Integration with other aftertreatment technologies (e.g. **SCR on Filters**)
- 4) **Ammonia slip** from SCR converters



## Aftertreatment converters models

axisuite						
software module	functionality / reactor type	3-way catalyst	diesel oxidation catalyst	lean NO <sub>x</sub> trap	selective catalytic reduction	diesel particulate filter
<i>axi</i> cat	 flow-through	✓	✓	✓	✓	n/a
<i>axi</i> trap	 wall-flow	n/a	✓	✓	✓	✓
<i>axi</i> heat	 exhaust pipe	single-wall	double-wall	insulating material	flanges	reacting flow

**Channel gas balances energy/species**

$$\rho_s v_s \frac{\partial T_s}{\partial x} = h \left( \frac{S}{\epsilon} \right) (T_s - T_c)$$

$$\frac{\partial (v_s S_i)}{\partial x} = -k_j \left( \frac{S}{\epsilon} \right) (c_{s,i} - c_{c,i})$$

**3-d solid energy balance**

$$\rho_s c_{p,s} \frac{\partial T_s}{\partial x} = k_{c,w} \frac{\partial^2 T_s}{\partial x^2} + k_{c,y} \frac{\partial^2 T_s}{\partial y^2} + k_{c,z} \frac{\partial^2 T_s}{\partial z^2} + S$$

**Filter scales 3-d solid energy balance**

$$\rho_s C_{p,s} \frac{\partial T_s}{\partial t} = k_{c,w} \frac{\partial^2 T_s}{\partial x^2} + k_{c,y} \frac{\partial^2 T_s}{\partial y^2} + k_{c,z} \frac{\partial^2 T_s}{\partial z^2} + S$$

$$S = H_{\text{trap}} + H_{\text{soot}} + H_{\text{spec}} + H_{\text{red}}$$

**Surface species**

$$\frac{\partial c_{s,i}}{\partial t} = R_i$$

**Wall/soot scale balances**

Mass/species

$$\frac{\partial c_{w,i}}{\partial t} = -R_i + \sum_j R_{j \rightarrow i} - \sum_k R_{i \rightarrow k}$$

Energy

$$\frac{\partial T_w}{\partial t} = \frac{1}{\rho_w c_{p,w}} \left( \sum_j R_{j \rightarrow i} h_{j,w} - \sum_k R_{i \rightarrow k} h_{i,w} \right) + \frac{1}{\rho_w c_{p,w}} \left( \sum_j R_{j \rightarrow i} h_{j,w} - \sum_k R_{i \rightarrow k} h_{i,w} \right)$$

**Global scale gas balances**


Mass/species

$$\frac{\partial (V_i \rho_i)}{\partial t} = (-1)^i \rho_i \mu_i A_i$$

Energy

$$\frac{\partial T_c}{\partial t} = \frac{\partial (T_c \rho_c)}{\partial t} = -\rho_c \mu_c A_c$$


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# Simulation Results

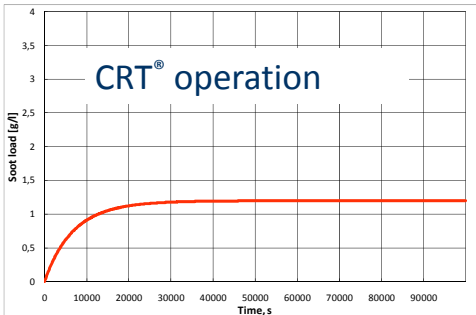
## A modeling study of soot and de-NO<sub>x</sub> reaction phenomena in SCR systems

SAE Technical Paper 2011-37-0031



## Concept analysis of CRT<sup>®</sup> operation






**CRT<sup>®</sup> operation**


**CRT<sup>®</sup>:**

- Continuously Regenerating Trap
- DOC + DPF system
- NO<sub>2</sub> from the DOC continuously regenerates the filter


Is CRT<sup>®</sup> applicable also for SCRF systems?



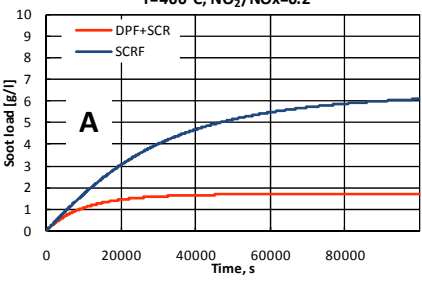
SAE Technical Paper 2011-37-0031



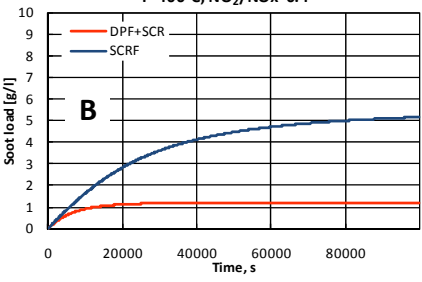
## Concept analysis of CRT<sup>®</sup> operation



**T=400°C; NO<sub>2</sub>/NO<sub>x</sub>=0.2**



**T=400°C; NO<sub>2</sub>/NO<sub>x</sub>=0.4**



**Simulated conditions:**

- 500 ppm NH<sub>3</sub>, 500 ppm NO<sub>x</sub>, NO<sub>2</sub>/NO<sub>x</sub>= 0.2, 0.4;
- 8%O<sub>2</sub>, 8%H<sub>2</sub>O,
- soot emissions= 1e-5 kg<sub>PM</sub>/kg<sub>exhausts</sub>
- mass flow rate=0.2235 kg/s
- NO<sub>2</sub>/soot mass ratio=16.5, 33
- Temperature: 400°C


Asymptotic value of soot load:

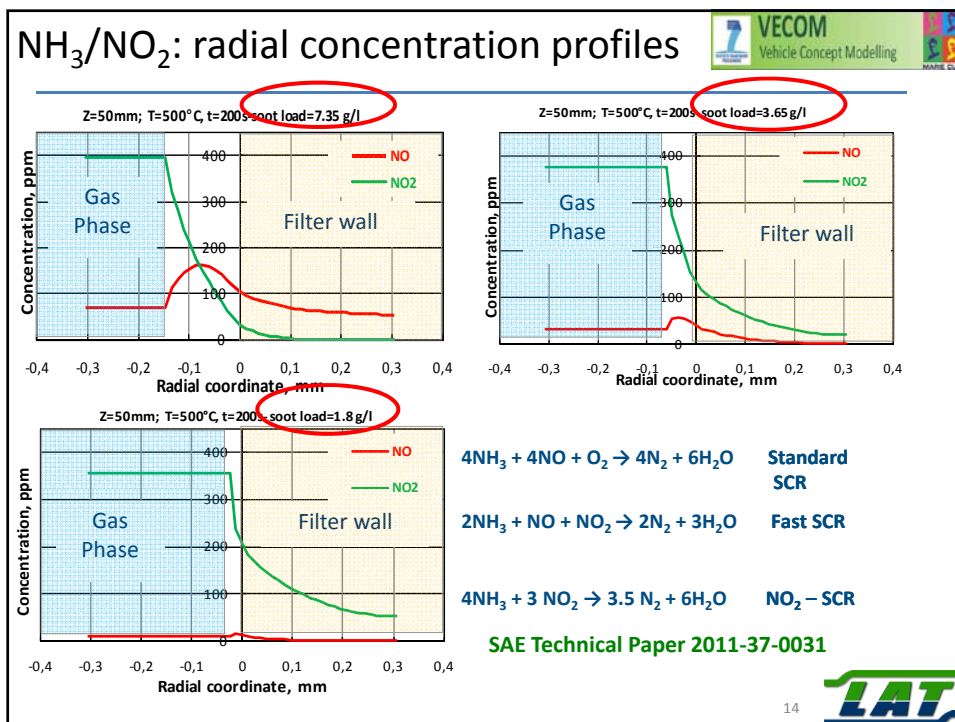
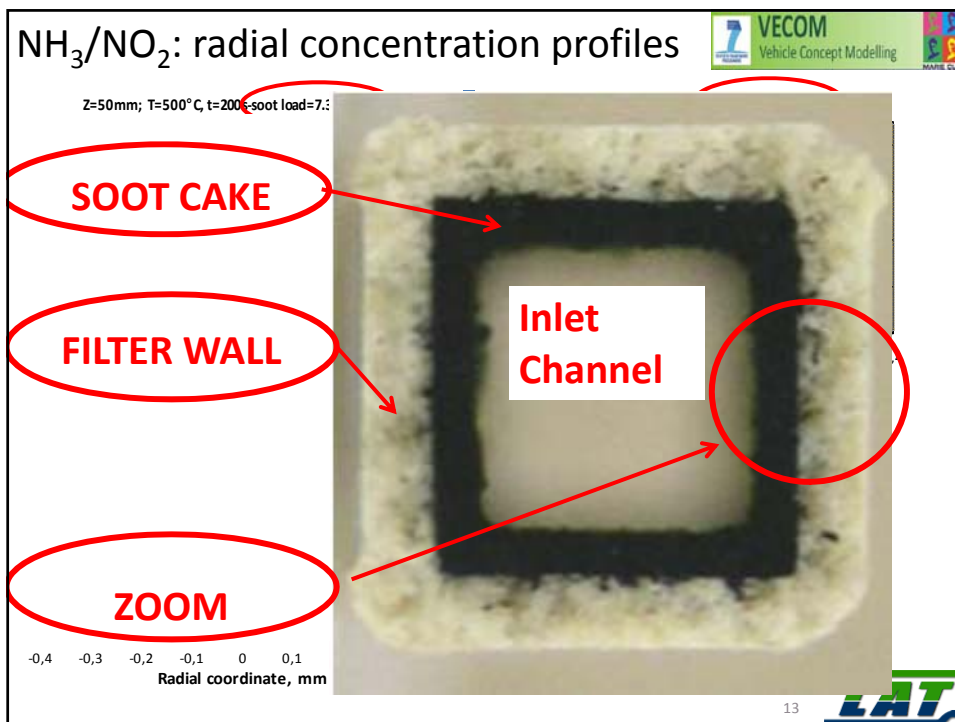
- Approached for the DPF+SCR configuration
- Approached also for SCRF


BUT high soot load → too high ΔP

**Different operating conditions required for CRT<sup>®</sup> operation over SCRF**

SAE Technical Paper 2011-37-0031









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## Simulation Results

### A novel approach to the modeling of dual-layer ammonia slip catalysts

CLEERS Workshop 2011,  
 In collaboration with Politecnico di Milano

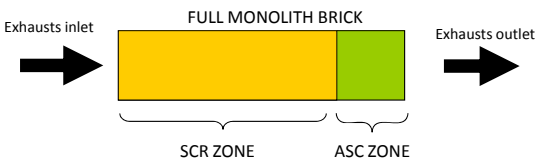




### Dual Layer ASCs concept\*

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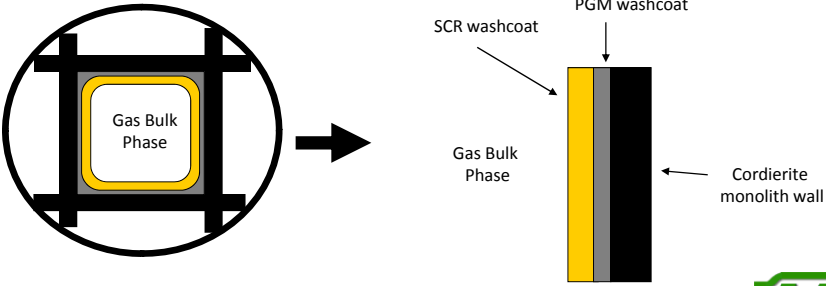
#### System configuration




FULL MONOLITH BRICK  
 SCR ZONE      ASC ZONE

ASC ZONE → double coated : SCR + PGM  
 → Improvement of  $\text{NH}_3$  conversion &  $\text{N}_2$  selectivity with SCR layer

#### Monolith Channel



Gas Bulk Phase  
 SCR washcoat  
 PGM washcoat  
 Gas Bulk Phase  
 Cordierite monolith wall



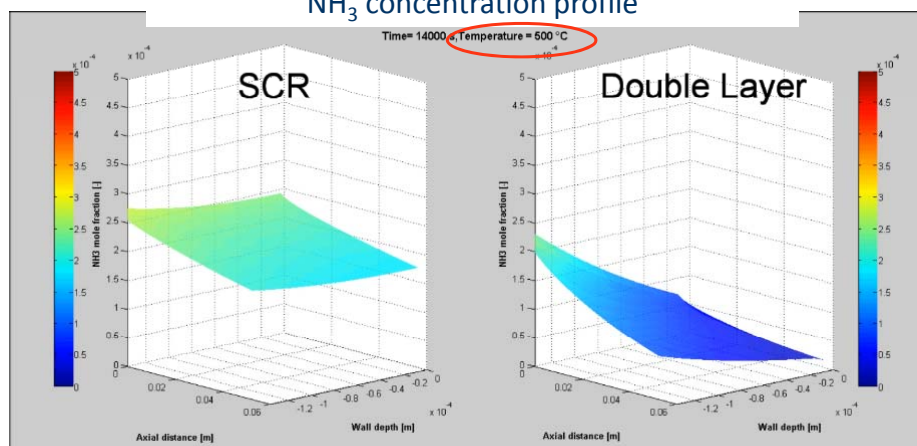
\* Scheuer et al. ICEC 2010, Beijing, China, September 12<sup>th</sup>-15<sup>th</sup> 2010 16

# How to model Dual-Layer ASC??

Is it necessary to model reaction/diffusion in both catalytic layers?

## SCR layer: effect of PGM addition

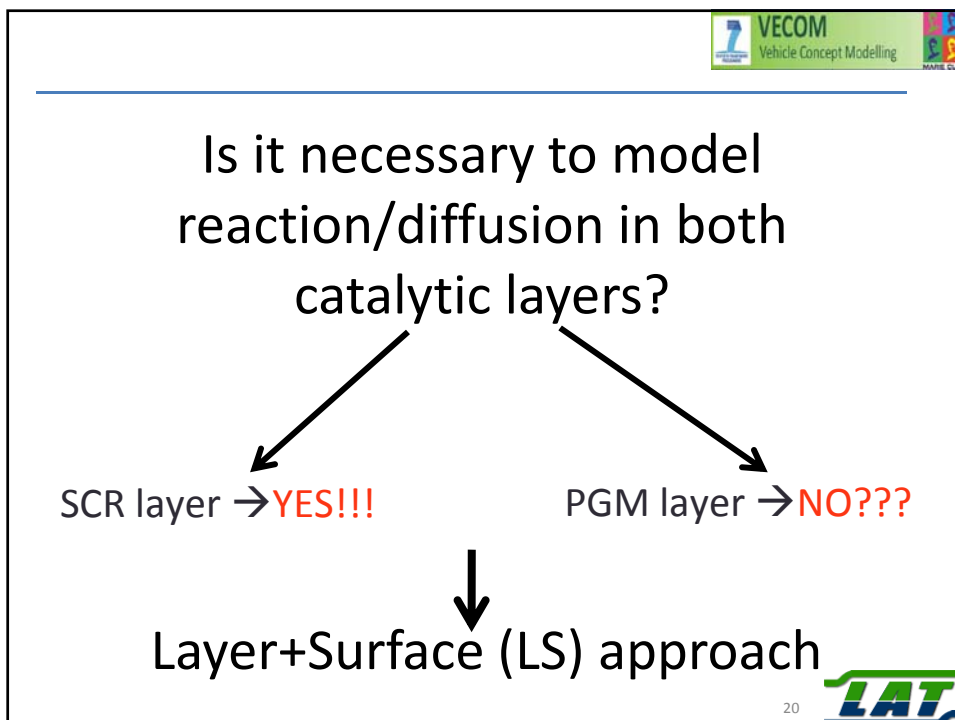
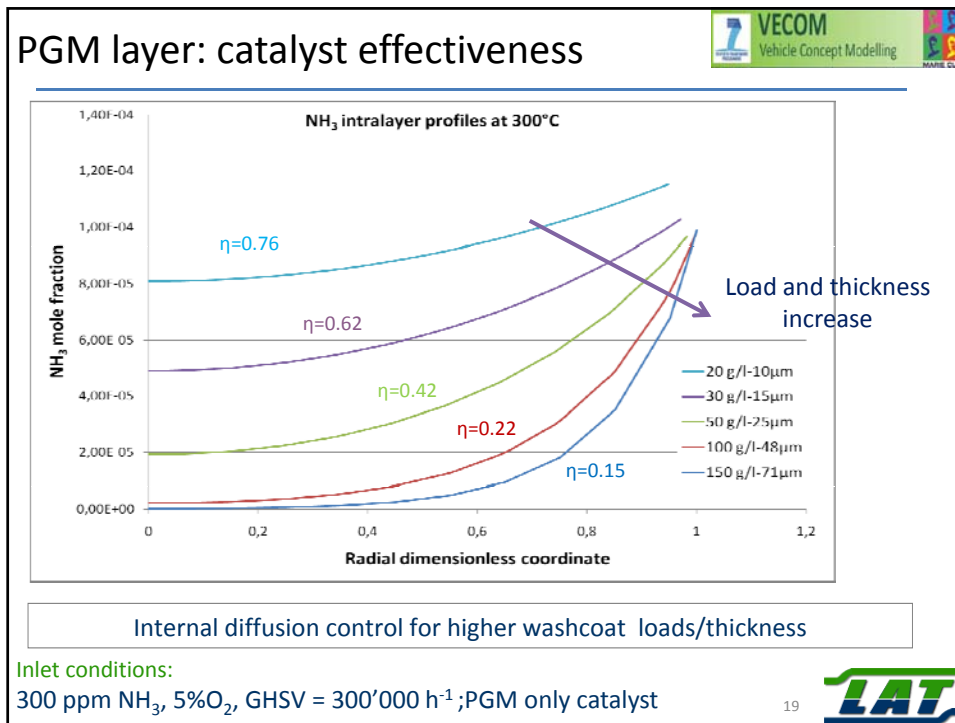
$\text{NH}_3/\text{NO}/\text{O}_2$  reacting system  
 $\text{NH}_3$  concentration profile

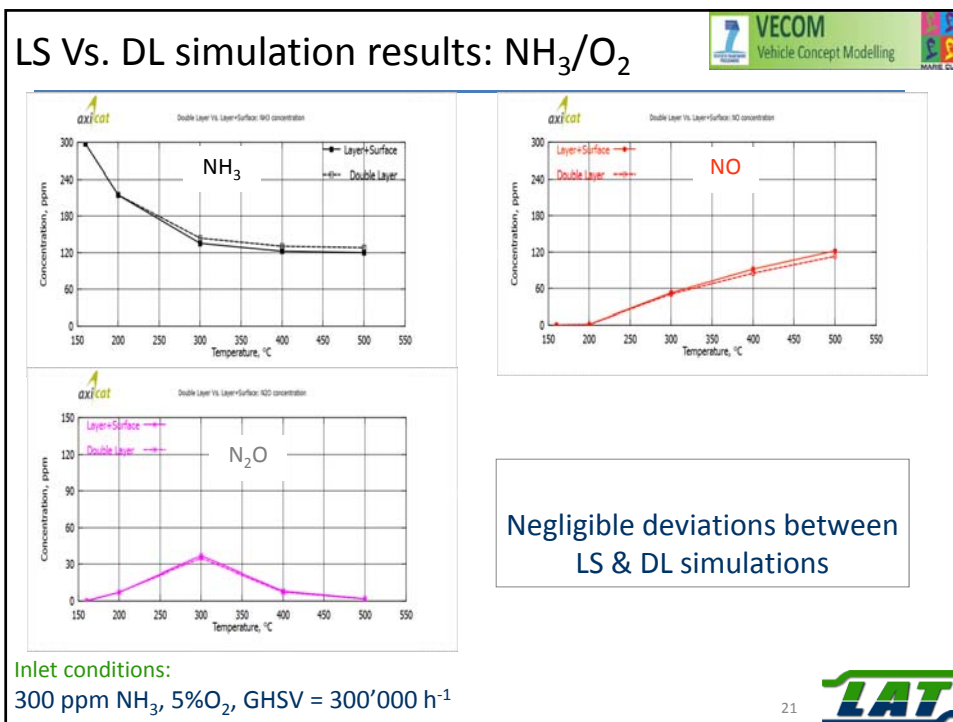


Colombo, Nova, Tronconi: Paper in preparation

Inlet conditions:

300 ppm  $\text{NH}_3$ , 300 ppm  $\text{NO}$ , 5%  $\text{O}_2$ , GHSV = 300'000  $\text{h}^{-1}$







## VECOM

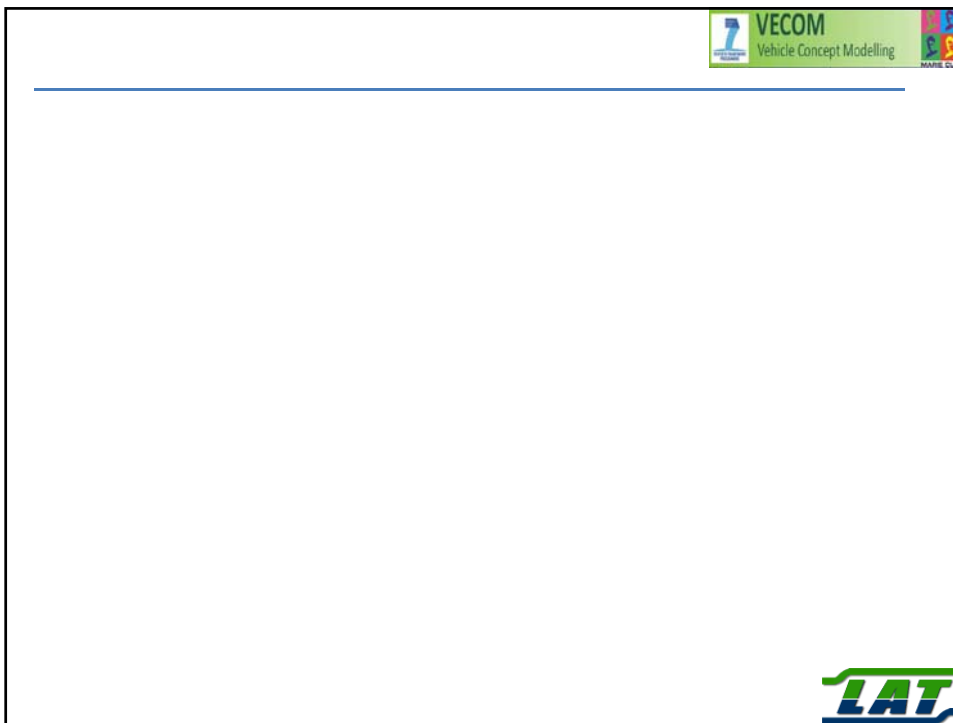
Vehicle Concept Modelling



# Thank you for your kind attention

mcolombo@aut.gr





### Dual layer ASCs concept

Why a dual layer system?

PGM catalysts have poor selectivity to  $N_2$

↓

The unselective oxidation products are  $N_2O$  and  $NO_x$ , which have to diffuse back in the SCR layer

↓

$NO_x$  can react with  $NH_3$  over the SCR catalyst to give  $N_2$ !!!

↓

Both  $NH_3$  conversion & selectivity to  $N_2$  increase

- Scheuer et al. Top.Catal. 52-2009-1847  
 - Scheuer et al. ICEC 2010, Beijing, China, September 12<sup>th</sup>-15<sup>th</sup> 2010

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